

IN THE CLAIMS:

Please amend the claims as follows:

1. (Currently Amended) A process in gaseous phase to obtain CFC 113a starting from CFC 113, wherein CFC 113, optionally diluted with a gas inert under the reaction conditions, is let flow on a catalyst consisting of aluminum fluoride in a fixed or fluidized bed at a reaction temperature of from 50°C to less than 200 °C.
2. (Original) A process according to claim 1, wherein CFC 113 is used in admixture with CFC 113a.
3. (Previously Amended) A process according to claim 1, wherein the fed CFC 113 amount, expressed as weight ratio between CFC 113/(catalyst x hour), is in the range 0.5-1.5.
- 4 (Currently Amended) A process according to claim 1, ~~wherein the reaction temperature is in the range 50°C—280°C~~ wherein the aluminum fluoride is obtained by fluorination of aluminum oxide with anhydrous hydrogen fluoride so that the introduced fluorine amount corresponds to 95% by weight or more.
5. (Currently Amended) A process according to claim 4, wherein the reaction temperature is ~~in the range 100°C—200°C~~ at least 100 °C.

6. (Previously Added). A process according to claim 5, wherein the reaction temperature is in the range 100°C - 160°C.

7. (New) A process according to claim 1, wherein the content of residual CFC-113 in the reaction mixture is lower than 1% by weight based on CFC-113a and CFC-113 present in the mixture.

8. (New) A process in gaseous phase to obtain CFC 113a starting from CFC 113, wherein CFC 113, optionally diluted with a gas inert under reaction conditions, is let flow on a catalyst consisting of aluminum fluoride in a fixed or fluidized bed at a reaction temperature of from 50°C to about 183°C, wherein the content of CFC-113a in the reaction mixture is at least 77.73% by weight.

9. (New) A process according to claim 8, wherein CFC 113 is used in admixture with CFC 113a.

10. (New) A process according to claim 8, wherein the fed CFC 113 amount, expressed as weight ratio between CFC 113/(catalyst x hour), is in the range 0.5-1.5.

11. (New) A process according to claim 8, wherein the aluminum fluoride is obtained by fluorination of aluminum oxide with anhydrous hydrogen fluoride so that the introduced fluorine amount corresponds to 95% by weight or more.

12. (New) A process according to claim 11, wherein the reaction temperature is at least 100 °C.

13. (New) A process according to claim 12, wherein the reaction temperature is in the range 100°C - 160°C.

14. (New) A process according to claim 8, wherein the content of residual CFC-113 in the reaction mixture is lower than 1% by weight based on CFC-113a and CFC-113 present in the mixture.

15. (New) A process according to claim 8, wherein the content of CFC-113a in the reaction mixture is at most 0.97% by weight.

16. (New) A process in gaseous phase to obtain CFC 113a starting from CFC 113, wherein CFC 113, optionally diluted with a gas inert under reaction conditions, is let flow on a catalyst consisting of aluminum fluoride in a fixed or fluidized bed at a reaction temperature of from 100°C to 160°C, wherein the content of residual CFC-113 in the reaction mixture is less than or equal to 0.9% by weight based on CFC-113a and CFC-113 present in the mixture.

17. (New) A process according to claim 16, wherein CFC 113 is used in admixture with CFC 113a.

18. (New) A process according to claim 16, wherein the fed CFC 113 amount, expressed as weight ratio between CFC 113/(catalyst x hour), is in the range 0.5-1.5.

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19 (New) A process according to claim 16, wherein the aluminum fluoride is obtained by fluorination of aluminum oxide with anhydrous hydrogen fluoride so that the introduced fluorine amount corresponds to 95% by weight or more.
